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Original Paper

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Numerical study of inhibition mechanism of high-pressure hydrogen leakage self-ignition with the addition of ammonia



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ABSTRACT

Hydrogen and ammonia have attracted increasing attention as carbon-free fuels. Ammonia is considered to be an effective energy storage and hydrogen storage medium. However, a small amount of unremoved NH₃ is still present in the product during the decomposition of ammonia to produce hydrogen. Therefore, it is very essential to investigate the self-ignition of hydrogen-ammonia mixtures in order to accommodate the various scenarios of hydrogen energy applications. In this paper, the effect of NH₃ addition on the self-ignition of high-pressure hydrogen release is numerically investigated. The RNG k- ϵ turbulence model, EDC combustion model, and 213-step detailed NH₃/H₂ combustion mechanism are used. CHEMKIN-Pro programs for zero-dimensional homogeneous and constant volume adiabatic reactor models are used for sensitivity analysis and ignition delay time of the chemical reaction mechanism. The results showed that the minimum burst pressure required for self-ignition increased significantly after the addition of ammonia concentration. The ignition delay time and H, HO₂, and OH radicals reduce with increasing ammonia concentration. H and HO₂ radicals are suggested as indicators for tracking the second and third flame branches, respectively.

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1. Introduction

Hydrogen has been considered as the most future energy due to its clean, environmental protection, low carbon, and other advantages (Gielen et al., 2019; Zhu et al., 2022a). At present, highpressure storage by gaseous hydrogen is the most widespread method for hydrogen storage with relatively simple and inexpensive technology (Usman, 2022). However, high-pressure tanks may cause uncontrolled hydrogen release due to tank bursts, punctures, tank overheating, etc. (Rudy et al., 2017). High-pressure hydrogen leakage into the air without clearly identifiable ignition sources

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may cause self-ignition, which will further lead to jet fires, explosions, etc. (Zhang et al., 2020).

In recent years, some scholars had proposed five hypothetical inferences for the mechanism of hydrogen self-ignition (Astbury and Hawksworth, 2007): (1) Reverse Joule-Thomson effect, (2) Hot surface ignition, (3) Sudden adiabatic compression, (4) Electrostatic ignition, and (5) Diffusion ignition. Of these mechanisms, diffusion ignition is widely accepted and researched by current researchers.

Recently, many scholars have investigated the numerous factors causing hydrogen self-ignition based on the diffusion ignition mechanism. The study found that hydrogen self-ignition was influenced by the boundary layer (Asahara et al., 2014; Xu et al., 2020), the diameter of the tube and its length (Duan et al., 2018; Jin et al., 2021; Kitabayashi et al., 2013), the release pressure (Asahara et al., 2022; Duan et al., 2019), the tube cross-section (Asahara et al., 2023; Li et al., 2019), the tube with different inlet

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Fig. 1. Geometric model of the experimental setup.

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Table 1 Boundary conditions

Parameters	Boundary condition
Inlet	Pressure-inlet boundary
Outlet	Pressure-outlet boundary
Inlet species	Pure hydrogen
Burst disk	Interior, open instantaneously
Tank and tube top wall	No slip wall, adiabatic boundary
Tank and tube lower wall	Axis
Temperature, K	300

shapes (Zhang et al., 2022), the diaphragm process (Asahara et al., 2021; Gong et al., 2019a; Kaneko and Ishii, 2016), the geometries of the downstream tube (Gong et al., 2016; Jin et al., 2022; Li et al., 2021b; Pan et al., 2020; Wang et al., 2020a, 2020b; Xu and Wen, 2014), and the obstacles inside the pipeline (Li et al., 2021a, 2022; Morii et al., 2015), etc. To further reveal the pattern of self-ignition occurrence and flame propagation when hydrogen was suddenly released into the downstream pipeline. Kim et al. (2013) completely documented the formation of self-ignition flame in the rectangular transparent tube and discovered that self-ignition occurs first in the boundary layer, and then the flame propagates along the boundary layer toward the front and tail of the mixing zone.

The above-mentioned study investigated the self-ignition of pure hydrogen. However, the future scenarios of hydrogen energy applications are becoming more and more diverse. Therefore, some scholars have investigated the influence of adding other gases on hydrogen self-ignition. For instance, several scholars have experimentally investigated the effects of adding methane (CH₄) (Rudy et al., 2014; Zeng et al., 2020a, 2020b), carbon dioxide (CO₂) (Gong et al., 2019b), nitrogen (N₂) (Rudy et al., 2017; Zeng et al., 2022a), and carbon monoxide (CO) (Zeng et al., 2022b) on the high-pressure hydrogen self-ignition. They discovered that the selfignition of high-pressure hydrogen was effectively suppressed by the addition of CH₄, CO₂, N₂, and CO. To further reveal the microkinetic properties of the effect of gas addition on hydrogen selfignition. Zhong and Gou. (2021) revealed the diffusion ignition of a pressurized H₂/CH₄ jet produced by the accidental release through numerical simulation methods. Although several scholars have investigated the effect of adding inert (N2, CO2, CO) or

	1800 -				Exp., P _{burst} = 7.09 Sim., P _{burst} = 7.09	MPa MPa
	- 1600 -			• 	Exp., $P_{burst} = 6.04$ Sim., $P_{burst} = 6.04$	MPa MPa
	1400 -					
ty, m/s	1200 -	Q				
/eloci	1000 -	V ₁		V ₂	C	, 3
-	800 -					
	600 -					
	400 -					
	200			400		
	100	200	Distan	ce, mm	000	000

Fig. 2. Comparison of experiment and simulation.

combustible (CH₄) gases on hydrogen self-ignition, there is still a serious lack of studies on the effect of other combustible gases on the self-ignition of hydrogen. In particular, there are few reports in the field of numerical simulation. At present, H₂ and NH₃ have attracted increasing attention as carbon-free fuels (Sun et al., 2022). In the ammonia-hydrogen energy roadmap for carbon neutrality, hydrogen was produced by the decomposition of ammonia, and a small amount of unremoved NH₃ was still present in the product stream (Jiang and Fu, 2021). However, there is a lack of analytical studies on the influence of NH₃ addition on hydrogen self-ignition. Therefore, it is essential to study the effect of adding NH₃ on high-pressure hydrogen self-ignition.

Some researchers took the OH mole fraction >0.001 as the criterion for the occurrence of high-pressure hydrogen self-ignition (Bragin et al., 2013; Bragin and Molkov, 2011; Gong et al., 2020). In addition, OH radicals were used to identify the flame front. However, the indicator for tracking the flame front may change

Table 2	2			
Major	parameters	in	numerical	simulations.

Name	Parameters						
Domain	2D-axis						
Solver	Double-precision, pressure-based, transient						
Mixture gas	Ideal gas						
Thermal conductivity, viscosity, and density	Ideal-gas-mixing-law						
Turbulent model	RNG k - e model						
Combustion model	Species transport with finite-rate model and EDC combustion model						
Chemical reaction kinetic mechanism	213-step NH ₃ /H ₂ reaction mechanism						
Discretization scheme	Pressure-velocity coupling, PISO algorithm, the second-order upwind scheme						
Time step, s	10 ⁻⁹						
Ignition delay time, normalized sensitivity	Constant volume zero-dimensional homogeneous adiabatic reactor						



Fig. 3. Physical model.



Fig. 4. Grid-independence analysis.

when other gases were added. For instance, Zhu et al. (2022b)

compared the evolution of the OH radical, H radical, HO₂ radical, and heat release rates (HRR), noting that the H radical had a good trend of change with HRR and recommended the H radical as an indicator to indicate the flame front. In addition, Zhong and Gou. (2021) also considered the OH and HO₂ radicals as good indicators for tracking the branching flame of hydrogen self-ignition. The results show that at low mixture fractions, OH radicals indicate a diffusion flame, and at high mixture fractions, HO radicals indicate a partially premixed flame. In summary, the indicators capturing the branch flame of hydrogen self-ignition may change after the addition of ammonia to hydrogen.

To further reveal the influence of ammonia addition on hydrogen self-ignition. In this work, a two-dimensional axisymmetric model was developed based on the computational fluid dynamics (CFD) approach. The RNG k-e turbulence model, the Eddy Dissipation Concept (EDC) model, and the 213-step detailed combustion reaction kinetic mechanism are used. The influence of ammonia addition on hydrogen self-ignition and shock wave propagation is numerically investigated. In addition, species tracking the flame front are discussed. As well, a sensitivity analysis of the chemical reaction mechanism is performed.



Fig. 5. The pressure curves for different concentrations of NH₃ addition inside the tubes.



Fig. 6. Theoretical pressure, temperature, and shock Mach behind the shock wave and shock wave velocity.

2. Numerical methods

2.1. Numerical schemes

At present, there are no experimental and simulation studies on the influence of ammonia addition on hydrogen self-ignition. Therefore, the high-pressure hydrogen self-ignition experiment by Xu et al. (2020) was chosen to validate the model. Since phenomena such as hydrogen self-ignition and shock wave propagation occur only in the downstream tube, the high-pressure tank in the simulation was simplified as in Xu et al. (2020). The computational domain was shown in Fig. 1. After the gridindependent simulation, a grid with 27075 cells was used in the subsequent calculation. The boundary conditions used in the simulations were summarized in Table 1.

In this work, Fluent 18.0 was used as the calculation tool and the finite volume method was employed to solve the 2D-axis Unsteady Reynolds Averaged Navier-Stokes (URANS) equations for a compressible Newtonian fluid. The 213-step detailed chemical reaction kinetic mechanism (Otomo et al., 2018) was chosen to simulate the chemical reaction of NH_3/H_2 in air and handle



Fig. 7. Variation of the maximum temperature inside the tube with different ammonia concentration additions.



Fig. 8. Burst pressure for self-ignition to occur at different NH_3 concentration additions.

Petroleum Science 20 (2023) 3184-3193

0% N	H ₃		1.85	iE-05 2.38	-05 2.75	E-05 3.2E	-05 3.65	E-05 4.1E	-05 4.55	E-05 5E	-05	5% N	H_3		1.85	E-05 2.38	-05 2.7	5E-05 3.2	E-05 3.6	5E-05 4.11	E-05 4.55	E-05 5E-	-05
580 µ	IS											600	μs										
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
_			0.00	1 0.0012 (0.0014 0.0	016 0.0018	0.002 0	0.0022 0.00	24 0.0026	6 0.0028 0	0.003	_			0.00	1 0.0011	0.0012 0.	0013 0.001	4 0.0015	0.0016 0.0	017 0.001	3 0.0019 0	0.002
590 µ	IS			× 0.55								610	μs				,	0.560 m					
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
			0.00	1 0.0028 (0.0046 0.0	064 0.0082	0.01 0	0.0118 0.01	36 0.0154	0.0172 0	0.019				0.00	1 0.0026	0.0042 0.	0058 0.007	4 0.009	0.0106 0.0	122 0.013	3 0.0154 0	0.017
600 µ	IS			\geq	33	3						620	μs					>	\leq				
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
10 /01	113				4E-1	05 6E-05	8E-05	0.0001	0.00012 0	.00014 0.0	0016	1370	1113		1.3	75E-05 2.	625E-05	3.5E-05	4.375E-	05 5.25E-I	05 6.125E	-05 7E-	-05
620 µ	IS											640	μs										
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
					0.00	1 0.002 0.0	03 0.004 0	0.005 0.008	0.007 0.	008 0.009	0.01					0.001 0.00	0105 0.0	011 0.001	15 0.001	0.00125	0.0013 (.00135 0.1	0014
630 µ	IS					~).565 m					650	μs							∠°.	574 m		
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
					0.00	1 0.003 0.0	05 0.007 0	0.009 0.011	0.013 0.1	015 0.017	0.019				0.00	1 0.0024	0.0038 0.	0052 0.006	6 0.008	0.0094 0.0	108 0.012	: 0.0136 C	0.015
640 µ	IS					2		2			,	660	μs				,		,.			5	
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59 DH mc	0.535 ble fract	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
					_					()							_						
0% NI	H ₃				30	0 420 54	0 660 7	80 900 1	020 1140	1260 1380	1500	5% N	NH3				3	100 420 5	540 660	780 900	1020 1140	1260 1380	1500
580 µ	IS											600	μs										
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
_				_	30	0 430 58	0 690 8	20 950 1	080 1210	1340 1470	1600						3	100 430 5	560 690	820 950	1080 1210	1340 1470	1600
590 µ	IS											610	μs										
0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59	0.535	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59
					30	0 510 72	0 930 11	40 1350 1	560 1770	1980 2190	2400						3	100 510 7	720 930	1140 1350	1560 1770	1980 2190	2400
600 µ	IS			\geq	-							620	μs						\leq				
0.535 10% N	0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.58	0.585	0.59		0.54	0.545	0.55	0.555	0.56	0.565	0.57	0.575	0.59		0.59
	NH2						0.01					0.535	NH ₂								0.00	0.585	
	NH3				30	0 420 54	0 660 7	80 900 1	020 1140	1260 1380	1500	^{0.535} 15%	NH ₃				3	100 420 5	540 660	780 900	1020 1140	1260 1380	1500
620 µ	NH ₃				30	0 420 54	0 660 7	80 900 1	020 1140	1260 1380	1500	0.535 15% 640	NH ₃				3	100 420 5	540 660	780 900	1020 1140	1260 1380	1500
620 µ 0.535	NH3 15 0.54	0.545	0.55	0.555	0.56	0 420 54	0 660 7	80 900 11 0.575	020 1140 0.58	0.585	0.59	0.535 15% 640 0.535	NH ₃ µs	0.545	0.55	0.555	0.56	0.565	540 660 0.57	0.575	0.58	0.585	0.59
620 µ 0.535	NH ₃ 15 0.54	0.545	0.55	0.555	30 0.56 30	0 420 54	0 660 7 0.57 0 810 9	80 900 11 0.575 80 1150 12	020 1140 0.58 320 1490	1260 1380 0.585 1660 1830	0.59	0.535 15% 640 0.535	NH ₃ µs	0.545	0.55	0.555	0.56	0.565	540 660 0.57 560 690	780 900 0.575 820 950	0.58	0.585	0.59
620 µ 0.535	NH3 IS 0.54	0.545	0.55	0.555	30 0.56 30	0 420 54	0 660 7	0.575 80 1150 12	020 1140 0.58 320 1490	0.585	1500	0.535 15% 640 0.535	NH ₃ µs	0.545	0.55	0.555	0.56	00 420 5	540 660 0.57 560 690	780 900 0.575 820 950	0.58	0.585	0.59
620 μ 0.535 630 μ 0.535	NH3 0.54 0.54	0.545	0.55	0.555	30 0.56 0.56	0 420 54 0.565 0 470 64 0.565	0 660 7	0.575 0.575	020 1140	0.585	1500 0.59 2000 0.59	0.535 15% 640 0.535	NH ₃ µs 0.54 µs 0.54	0.545	0.55	0.555	3 0.56 3 0.56	0.565	540 660 0.57 560 690 0.57	780 900 0.575 820 950 0.575	0.58	0.585	0.59
620 μ 0.535 630 μ 0.535	NH3 0.54 0.54	0.545	0.55	0.555	30 0.56 0.56 0.56	0 420 54 0.565 0 470 64 0.565 0 540 78	0 660 7	80 900 11 0.575 80 1150 1 0.575 80 1500 1	0.58 0.58 0.58 0.58 0.58 740 1980	0.585 0.585 0.585 0.585 0.585	1500 0.59 2000 0.59 2700	0.535 15% 640 0.535 0.535	NH ₃ µs 0.54 µs 0.54	0.545	0.55	0.555	3 0.56 0.56	0.565	540 660 0.57 560 690 0.57 40 960	780 900 0.575 820 950 0.575 1180 1400	0.58	0.585 1260 1380 0.585 1340 1470 0.585 2060 2280	0.59
620 μ 0.535 630 μ 0.535	NH3 0.54 0.54	0.545	0.55	0.555	30 0.56 30 0.56	0 420 54 0.565 0 470 64 0.565 0 540 78	0 660 7	80 900 1 0.575 80 1150 1 0.575 80 1150 1	0.58	1260 1380 0.585 1660 1830 0.585 2220 2460	1500 0.59 2000 0.59 2700	0.535 15% 640 0.535 650 0.535	NH ₃ µs 0.54 µs µs	0.545	0.55	0.555	3 0.56 3 0.56	0.565	540 660 0.57 560 690 0.57 40 960	780 900 0.575 820 950 0.575 1180 1400	0.58	0.585	0.59

Fig. 9. The contour of OH mole fraction and temperature during self-ignition with different NH₃ concentration additions (P_{burst}: 7.0 MPa; Units: meter).

turbulence-chemistry interactions. Moreover, this mechanism contains a detailed H_2/O_2 chemical reaction mechanism. The species transport with the finite-rate model (Fluent, 2011) and EDC combustion model (Magnussen, 1981) were employed to handle the combustion reactions whereas the RNG *k-e* model (Yakhot and Orszag, 1986) was employed to simulate both high and low Reynolds number turbulence. For details see our previous paper (Li et al., 2022). To further explain the 213-step NH₃/H₂ chemical reaction kinetic mechanism, numerical simulations were carried out using the CHEMKIN-Pro program (Kee et al., 1996). A zero-dimensional (0-D) adiabatic reactor model with a constant volume was used. The numerical simulation details were summarized in Table 2.

2.2. Model validation

Fig. 2 shows the comparison between the numerical simulation results and the experimental data. The results show that the simulation results were in good agreement with the experimental data. In this work, hydrogen was considered the ideal gas, and the

burst disk was considered to rupture instantaneously. Therefore, the V_1 of the numerical simulation was always greater than the V_1 of the experimental results in the initial stage of the high-pressure hydrogen leakage, regardless of the burst pressure. When the burst pressure was relatively low ($P_{\text{burst}} = 6.04$ MPa), the shock wave intensity weakened and the shock wave velocity decreased accordingly due to the dissipation and attenuation of the shock wave (Xu et al., 2020). Therefore, the shock wave velocity was gradually reduced for both the numerical simulation and the experimental process. However, the numerically simulated shock wave velocity reduction trend was much faster. This was due to the superposition of compressional waves generated during the multistage rupture of the experimental burst disk which makes the shock wave velocity decrease slowly.

When the burst pressure was high ($P_{\text{burst}} = 7.09$ MPa), the compressional waves produced by the burst disk's multi-stage rupture process would have a significant superimposed effect and increase the propagation velocity of the shock waves (Asahara et al., 2021; Gong et al., 2019a; Kaneko and Ishii, 2016). Therefore, at

 $P_{\text{burst}} = 7.09$ MPa, the experimental V_2 was larger than the numerical simulation V_2 . After the rupture, the shock wave decays steadily, and the shock wave velocity gradually decreases. As a result, during the experiment, the shock wave's propagation velocity first rises and then gradually falls. However, in the numerical simulation, the velocity of the shock wave was always decreasing gradually. In conclusion, V_3 of the numerical simulation was smaller than V_3 of the experiment. In summary, there was a small discrepancy between the simulation results and the experimental results. In addition, the maximum average relative error between the numerical simulation results and the experimental data was 3.93%. Therefore, the CFD model used in this paper was correctly validated.

2.3. Model description

Researchers at the Warsaw University of Technology indicated that the self-ignition of high-pressure hydrogen was related to the length of the tube, but not to the diameter of the tube (Rudy et al., 2014, 2017). Therefore, the effect of diameter on hydrogen selfignition was neglected in this work, and the self-ignition of highpressure hydrogen in a 700 mm long tube with a diameter of 5 mm was investigated. The above-mentioned validated CFD model was used for simulations to study the effect of ammonia addition (0, 5, 10, and 15%) on the self-ignition of high-pressure hydrogen leakage. Fig. 3 shows the schematic diagram of the physical model. To ensure grid-independent simulations, a grid-independent analysis was performed by using several grid counts. It was found that the simulation results for the maximum temperature evolution ($P_{\text{burst}} = 7.0 \text{ MPa}$) changed very little when the number of grids was increased from 14480 to 16064, as shown in Fig. 4. Thus, the total number of grids eventually used was 14480.

3. Result and discussion

3.1. Effects of ammonia concentration on shock wave inside the tube

Fig. 5 shows the pressure curves at different locations in the tube for various ammonia concentration additions (The distances of P_1 , P_2 , P_3 , and P_4 from the burst disk are 300 mm, 400 mm, 500 mm, and 600 mm, respectively). The four cases have the same burst pressures of 8.50 MPa but have different NH₃ additions of 0%, 5%, 10%, and 15%. From Fig. 5, a sudden increase in pressure is successively detected by the four pressure monitoring points at the tube wall. It suggests that after the burst disk opens, a leading shock wave is produced and propagates along the downstream tube. Moreover, from Fig. 5(a)–(d), it is observed that the pressure in the tube gradually reduces with the increase of NH₃ concentration, which will inhibit the occurrence of self-ignition.

According to the usual one-dimension (1-D) shock tube theory (Gaydon and Hurle, 1963), the theoretical Mach number (M), pressure behind the shock wave (P_2), the temperature behind the shock wave (T_2), and shock wave velocity can be obtained in Eqs. (1)–(4):

$$\frac{P_4}{P_1} = \frac{2\gamma_1 M^2 - (\gamma_1 - 1)}{\gamma_1 + 1} \left[1 - \frac{\gamma_4 - 1}{\gamma_1 + 1} \frac{a_1}{a_4} \left(M - \frac{1}{M} \right) \right]^{-2\gamma_4/(\gamma_4 - 1)}$$
(1)

$$a_4 = (\gamma_4 R T_4 / M)^{1/2} \tag{2}$$



Fig. 10. Ignition delay times of $\rm H_2/\rm NH_3/\rm air$ with different ammonia concentration additions.

$$\frac{P_2}{P_1} = \frac{2\gamma_1 M^2 - (\gamma_1 - 1)}{\gamma_1 + 1}$$
(3)

$$\frac{T_2}{T_1} = \frac{\left[2\gamma_1 M^2 - (\gamma_1 - 1)\right] \left[(\gamma_1 - 1)M^2 + 2\right]}{(\gamma_1 + 1)^2 M^2}$$
(4)

where P_4 is the initial pressure in the high-pressure region, and P_1 is the initial pressure in the tube. T_1 and T_4 are the initial temperature in the tube and high-pressure region, respectively. r_1 and r_4 is the gas-specific heat ratio of air and ammonia/hydrogen mixture, respectively. a_1 and a_4 is the speed of sound in air and hydrogen/ ammonia mixture, respectively. According to Eq. (1), the addition of NH₃ affects the values of a_4 and r_4 in the mixture. Since the heat capacity ratios of the three gases (air, hydrogen, ammonia) are similar, the change in the heat capacity ratio of the mixture at



Fig. 11. Normalized sensitivity analysis of ignition delay time for various NH_3/H_2 mixtures at 1500 K and 7.0 MPa.



Fig. 12. H, OH, and HO₂ radical mole fraction profiles of hydrogen/ammonia mixture at 1600 K, 7.0 MPa, $Z_{mr} = 0.01$ (The solid line represents change with time; the dotted line represents change with temperature).

different ratios of hydrogen is negligible. However, the sonic speed in hydrogen/ammonia mixture with different NH_3 additions can be calculated as Eq. (2). In hydrogen/ammonia mixtures, increasing the concentration of ammonia will reduce the local sound speed. Fig. 6(a) shows the theoretical shock wave velocity for different concentrations of ammonia added to high-pressure hydrogen. Fig. 6(a), the shock wave velocity reduces as ammonia is added. Analogously, based on the 1-D shock tube theory, the pressure, temperature, and shock Mach behind the shock wave are displayed in Fig. 6(b), (c), and (d), respectively. The results show that the pressure, temperature, and shock Mach behind the shock wave reduce as more ammonia is added to the high-pressure hydrogen.

3.2. Effects of ammonia addition on self-ignition inside the tube

Fig. 7 shows the effect of different NH₃ concentration additions on the maximum temperature inside the tube. From Fig. 7, it can be found that the maximum temperature profiles for different NH₃ concentrations have a similar trend. The maximum temperature profile for 15% NH₃ concentration addition is used as an example. After the instantaneous rupture of the burst disk, the leading shock wave generated in the tube makes the first increase in the tube temperature within 0–38 μ s. At 38–645 μ s, the temperature inside the tube gradually increased with the propagation of the leading shock wave to the downstream tube. At 645–683 μ s, when selfignition takes place in the tube after the temperature jumps to about 3000 K in a very short period. At 683–725 μ s, the temperature increases slightly and then decreases slightly. After that, the temperature will gradually increase with time, which indicates the formation of a stable hydrogen flame in the tube. Moreover, as the NH₃ concentration increase, the maximum temperature inside the tube gradually decreased, and the occurrence time of self-ignition is gradually delayed.

Fig. 8 shows the minimum burst pressure for self-ignition to occur at different NH_3 concentration additions. In this work, the OH mole fraction >0.001 is considered a criterion for the occurrence of self-ignition (Bragin et al., 2013; Bragin and Molkov, 2011; Gong et al., 2020; Jin et al., 2021; Zhang et al., 2020). From Fig. 8, the minimum burst pressure of self-ignition to occur for 0% NH_3 is 3.62 MPa. However, for 5%, 10%, and 15% NH_3 addition, the values increase to 3.75, 3.83, and 3.90 MPa, respectively, which are 1.036, 1.058, and 1.077 times higher than in the case of 0%. The results show that the addition of ammonia will significantly improve the critical burst pressure for high-pressure hydrogen self-ignition to occur.

Fig. 9 shows the contour of OH mole fraction and temperature during self-ignition with different NH_3 concentration additions. As shown in Fig. 9, the initial self-ignition happens in the boundary layer at different NH_3 concentration additions. Then, the flame propagates around the boundary layer and reaches the front and tail of the mixing zone. Finally, a complete flame is formed around the mixing zone and moves downstream with the shock wave. However, when NH_3 concentration is added at 0%, 5%, 10%, and 15%, the distances between the burst disk and the location of self-ignition occurrence are about 0.552, 0.560, 0.565, and 0.574 m, respectively. Moreover, the self-ignition onset times were 590, 610, 630, and 650 μ s, respectively. Therefore, as the NH_3 concentration increases, the possibility of self-ignition occurs gradually decreases.

3.3. Effect of NH₃ addition on the chemical kinetic mechanism

The initial mass ratio of fuel versus air in the H₂/NH₃/air mixture is programmed to be higher than the most reactive mixture fraction $(Z_{mr} = 0.01)$ (Zhong and Gou, 2021). Fig. 10 shows the ignition delay time (IDT) versus the initial temperature for H₂/NH₃/air mixtures added with different ammonia concentrations. The initial pressure and initial temperature of the reactor are 7.0 MPa and 1000–1600 K, respectively. The results show that the ignition delay time of the H₂/NH₃ binary fuel decreases exponentially as the initial temperature increases. Moreover, the ignition delay time gradually increases with the NH₃ concentration increases, but the increase is not significant. This interesting phenomenon is similar to the influence of CH₄ adding on the self-ignition of pressurized hydrogen studied by Zhong and Gou (2021). Therefore, the results show that the addition of NH₃ has not caused significant changes in the high-pressure hydrogen ignition mechanism.

Fig. 11 shows the normalized sensitivity coefficient of the stoichiometric H₂/NH₃ mixture to the ignition delay time. A positive coefficient indicates that the response has a positive effect on the ignition delay time and vice versa. The initial temperature is 1500 K, the constant pressure is 7.0 MPa, and the mixing levels are 0, 0.05, 0.1, and 0.15. As shown in Fig. 11, the ignition delay time is strongly influenced by the chain-branching reactions $H+O_2 =$ O+OH (R1) and $H+O_2$ (+M) = HO₂ (+M) (R13). Moreover, under current conditions, the chain-branching reaction R1 is always the most significant chain-branching reaction producing many reactive radicals (O and OH), and also the most significant chain-branching reaction promoting the combustion of all hydrogen/ammonia mixtures. In contrast, the chain-branching reaction R13 has an obvious negative effect on the ignition delay time. This is because the chain-branching reaction R13 consumes the H radical and produces the stable intermediate radical HO₂. In addition, the sensitivity coefficients of all chain-branching reactions decrease with increasing the proportion of ammonia. Thus, the sensitivity of ignition delay time decreases gradually with increasing ammonia concentration.

3.4. Evolution of OH, HO₂, H, and HRR

As discussed in the sensitivity analysis above, the H, HO₂, and OH radicals have a significant effect on the chain-branching reaction during hydrogen ignition; therefore, it is necessary to investigate the effect of ammonia addition on the mole fractions of H, HO₂, and OH radicals. Meanwhile, the H, OH, and HO₂ radicals are strongly associated with hydrogen ignition. Fig. 12 shows the mole fraction profiles of H, HO₂, and OH radicals for different stoichiometric H₂/NH₃ mixtures. The initial temperature is 1500 K, the initial pressure is 7.0 MPa, and $Z_{mr} = 0.01$. From Fig. 12, the peak of H, HO₂, and OH radicals decreased with increasing the proportion of ammonia. In addition, the H and HO₂ radicals. In conclusion, the addition of ammonia decreases the accumulation of OH, HO₂, and H radicals.

In addition, studies by several scholars have shown that OH, HO₂, and H radicals could all capture the ignition kernel (Zhong and Gou, 2021; Zhu et al., 2022b). Therefore, in this section, indicators that can be used to track the flame branches of hydrogen self-ignition are investigated. Fig. 13 shows the variation of HRR, OH radicals, HO₂ radicals, and H radicals on the central axis of the tubes for different NH₃ concentrations. As shown in Fig. 13, compared to OH radical, the trends of H and HO₂ radicals mole fractions are more similar to the trends of HRR. It is found that the H and HO₂ radicals show three peak concentration accumulations inside the tube, which indicates that three separate flames are produced.



Fig. 13. HRR and mole fraction of H, HO₂, and OH radicals on the central axis in tubes of different NH_3 concentrations additions ($P_{burst} = 8.5$ MPa).

However, the OH radical showed only one peak concentration accumulation in the tube and could not show three separate flames. As shown in Fig. 13(a)-(c), it is found that the second peak concentration accumulations of H radicals are more obvious than the H and HO₂ radicals. Yet, the third peak concentration accumulations of the HO₂ radical are more obvious than the OH and H radicals. Therefore, the flame branches cannot be captured by only one of the OH, H, or HO₂ radicals. The results show that H and HO₂ radicals are good indicators for tracking the second and third flame branches, respectively, compared to OH radicals. At the same time, it can be observed that the peak of OH is in front of the peak of HRR. This is because in a shock tube-like channel where the air is in the low-pressure side and the fuel mixture will break the diaphragm, OH radicals will be formed in the front (heated gases are in the front when shock wave passed through), and because the fuel is behind the shock front, the flame will propagate against the propagation direction of the fuel gas mixture. Therefore, OH peaks in front of the HRR.

4. Conclusions

In this paper, the effect of NH₃ concentration additions (0%, 5%, 10%, and 15%) on the self-ignition of high-pressure hydrogen accidently released into the tube is numerically investigated. The species transport with finite-rate model and EDC combustion model is employed to study the combustion reactions whereas the RNG k-e model is used for the turbulence model, and the 213-step detailed hydrogen/ammonia chemical reaction kinetic mechanism is used. The mechanism of the effect of ammonia addition on the shock wave propagation, self-ignition occurrence, and combustion characteristics during the hydrogen self-ignition is elucidated. Moreover, the CHEMKIN-Pro program with the 0-D homogeneous and constant volume adiabatic reactor model performs a sensitivity analysis of the ignition delay time of the combustion reaction mechanism. The following conclusions are drawn.

- (1) The intensity and propagation velocity of the shock wave in the tube reduced with the increase of NH₃ concentration. Based on the 1-D shock theory, the shock wave intensity decreases and the temperature of the shock wave heating decreases accordingly, which is detrimental to the occurrence of self-ignition. The value of the critical burst pressure required for self-ignition to occur increases with the addition of NH₃ concentration. In addition, the possibility of selfignition decreased with increasing NH₃ concentration when the burst pressure is higher than the critical minimum burst pressure required for self-ignition to occur. Compared to the case of pure hydrogen, the critical burst pressure required for self-ignition may be increased by a factor of 1.036, 1.058, and 1.077 times for 5%, 10%, and 15% ammonia additions, respectively. As the concentration of NH₃ increases, the maximum temperature inside the tube gradually decreases and the onset of self-ignition is gradually delayed. With the increase of NH₃ concentration, the distance between the position where self-ignition occurs inside the tube and the burst disk gradually increases. However, regardless of the amount of ammonia added, the self-ignition inside the tube occurred at the tube wall.
- (2) Further explanation of the effect of NH₃ addition on the combustion kinetic mechanism of the H₂/NH₃ chemical reaction is provided. The ignition delay time gradually increases with increasing NH₃ concentration. The ignition delay time is most affected by the chain-branching reaction $H+O_2 = O+OH$ (R1), which promoted the combustion of the hydrogen/ammonia mixture. The chain-branching reaction $H+O_2$ (+M) = HO₂ (+M) (R13) has a significant negative effect on the ignition delay time, and the R13 plays a role in inhibiting self-ignition. The sensitivity coefficients for all chain-branching reactions decreased with increasing the proportion of NH₃. Therefore, the sensitivity of ignition delay time gradually reduces with the increase of NH₃ concentration.
- (3) The effect of ammonia addition on the flame propagation characteristics is investigated. The accumulation of OH radicals, H radicals, and HO₂ radicals decreases with increasing the proportion of NH₃. Three peak concentration accumulations are observed for the mole fraction profiles of H and HO₂ radicals, which indicated the generation of three separate flames. The mole fraction trends of HO₂ and H radicals are more similar to those of HRR than those of OH radicals. Therefore, H and HO₂ radicals are suggested as good indicators for tracking the flame branches of hydrogen selfignition compared to OH radicals. Moreover, based on the observed distinctness of the flame branches, H and HO₂

radicals are suggested as better indicators for tracking the second and third flame branches, respectively.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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